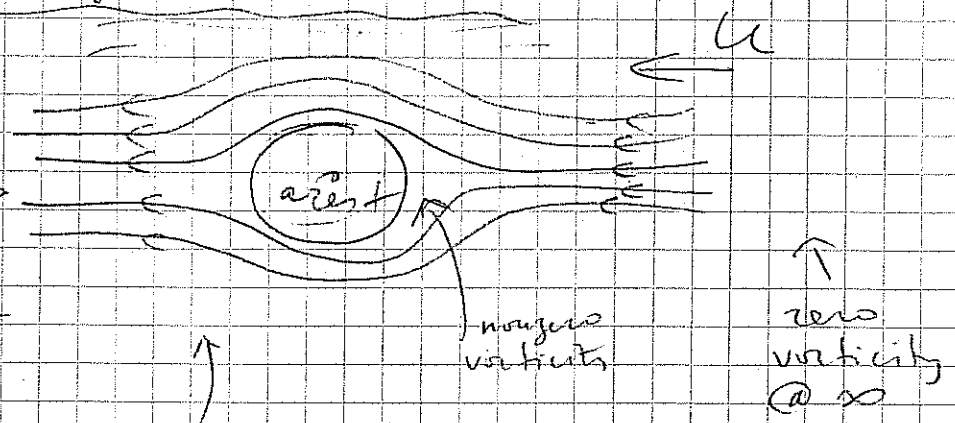


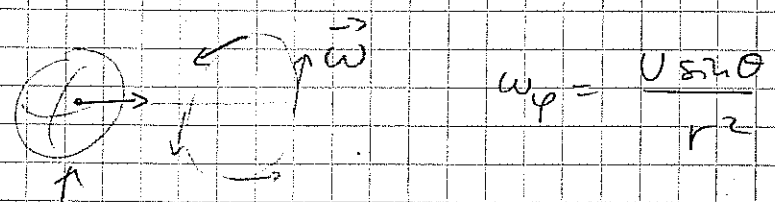
# What happens to the flow as $R \uparrow$ ?

\*  $R \ll 1$

qualitative picture good (incl improvement as  $r \rightarrow \infty$ )



\* remember this flow was described by  $\Delta \vec{\omega} = 0$ ,  $\vec{\omega} = w_\varphi \vec{e}_\varphi$

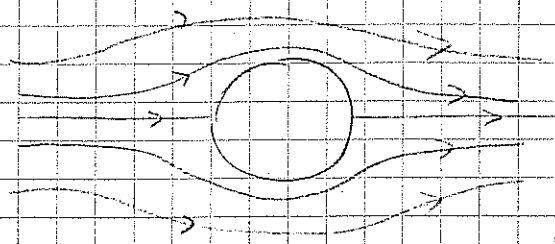


\* vorticity is generated at surface of the body by the dragging of the fluid and then diffuses away in all directions as if from a stationary source

this suggests that as  $R \uparrow$  asymmetry before-after will be more pronounced

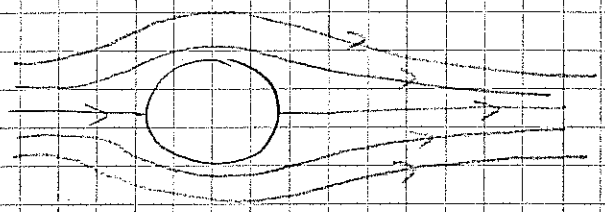
- + the flow, in the Stokes' eqns ( $R \ll 1$ ) approx is fore- and after-symmetric
- + in improved approximation, vorticity diffuses from a moving source, breaking the before-after symmetry, far away from the body (where Stokes' breaks down)

for a cylinder [experiments / numerical simulas]



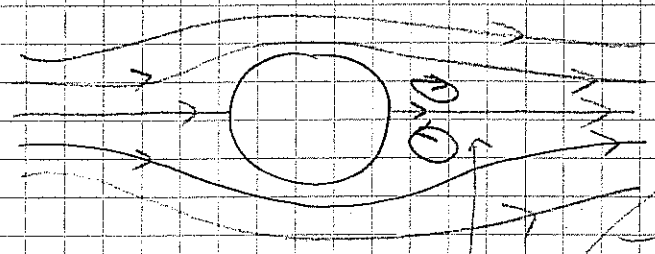
$R = 0.25$

(= fore/aft-symmetry)



$R \approx 3.5$

(fore/aft-symmetry gone)



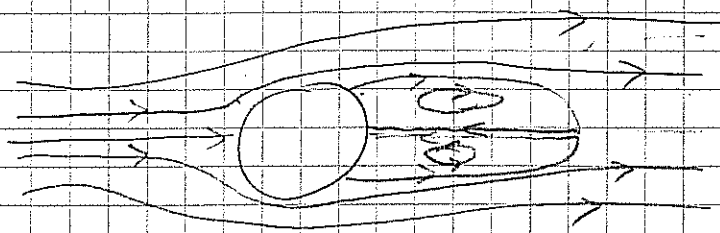
$R \sim 9$

"standing eddies"

(1st at  $R = 6$ ; appears then)

as  $R$  increases  
this region w/  
closed streamlines  
behind cylinder  
becomes larger & wider

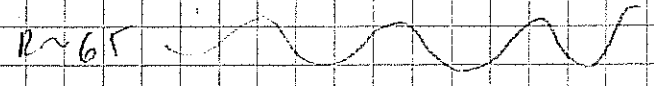
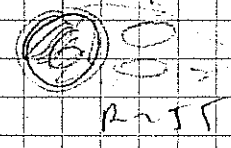
e.g.



$R = 70$  etc

drag at higher  $R$   
 $\sim \pi a^2 \frac{\rho U^2}{2} f(R) \sim a^2 \rho U^2$   
 ↓ ↓ variation  
 x-section of pressure  
 i.e.  $f(R) \sim \frac{1}{R}$  small  $R$ ,  $f(R) \sim$  const  
 layer  $R$   
 wave instability

In addition, for away



etc

So we're led to considering  
flows at large  $R$

it would appear that, as we did at  
 small- $R$  = drop inertia, keep  $v \Delta \vec{u}$   
 here, we could keep inertia & drop  $v \Delta \vec{u}$  - term

unfortunately, this does not  
 agree w/ what's observed

(this would imply that large- $R$  flows  
 $\equiv$  ideal fluid flows)

- main difference lies in effect of boundaries,  
 where  $v$  becomes relevant

- as we saw in sphere case, nontrivial  $\vec{\omega}$  (vorticity)  
 is generated @ boundaries & diffuses away  
 turns out that vorticity  $\vec{\omega}$  can not be created or  
 destroyed in interior of homogeneous fluid & is  
 produced @ boundaries.

so we begin by studying EOM for  $\vec{\omega}$ :

start w/ NS:

$$\rho \left( \frac{\partial \vec{u}}{\partial t} + (\vec{u} \cdot \nabla) \vec{u} \right) = \vec{F} - \nabla p + \mu \Delta \vec{u}$$

$$\text{let } \rho = \text{const}, \quad \nabla \cdot \vec{u} = 0$$

so

$$\frac{\partial \vec{u}}{\partial t} + (\vec{u} \cdot \nabla) \vec{u} = \frac{\vec{F}}{\rho} - \nabla \left( \frac{p}{\rho} \right) + \nu \Delta \vec{u}$$

some tricks - (GOAL - get eqn for  $\vec{\omega}$ )

$$\vec{u} \times (\vec{\nabla} \times \vec{u}) = \frac{1}{2} \vec{\nabla} (\vec{u} \cdot \vec{u}) - (\vec{u} \cdot \vec{\nabla}) \vec{u}$$

Proof

$$\begin{aligned} \epsilon^{ijk} u_j (\vec{\nabla} \times \vec{u})^k &= \epsilon^{ijk} u_j \epsilon^{klm} \partial^l u^m = \\ &= \epsilon^{ijk} \epsilon^{klm} u_j \partial^l u^m = \\ &= (\delta^{il} \delta^{jm} - \delta^{im} \delta^{jl}) u_j \partial^l u^m = \\ &= u^m \partial^i u^m - u^j \partial^j u^i \\ &= \frac{1}{2} \partial^i (u^m u^m) - (u^j \partial^j) u^i \quad \square \end{aligned}$$

hence  $(\vec{u} \cdot \vec{\nabla}) \vec{u} = -\vec{u} \times \vec{\omega} + \frac{1}{2} \vec{\nabla} (\vec{u}^2)$

plug into NS:

$$\frac{\partial \vec{u}}{\partial t} - \vec{u} \times \vec{\omega} = \frac{\vec{F}}{\rho} - \vec{\nabla} \left( \frac{p}{\rho} + \frac{1}{2} \vec{u}^2 \right) + \nu \Delta \vec{u}$$

take  $\vec{\nabla} \times (-)$

$$\begin{aligned} \frac{\partial \vec{\omega}}{\partial t} - \vec{\nabla} \times (\vec{u} \times \vec{\omega}) &= \vec{\nabla} \times \left( \frac{\vec{F}}{\rho} \right) - \vec{\nabla} \times \vec{\nabla} \left( \frac{p}{\rho} + \frac{1}{2} \vec{u}^2 \right) \\ &\quad + \nu \Delta (\vec{\nabla} \times \vec{u}) \end{aligned}$$

assume  $\vec{F} = \vec{\nabla} \psi$

$$\frac{\partial \vec{\omega}}{\partial t} - \vec{\nabla} \times (\vec{u} \times \vec{\omega}) = \nu \Delta \vec{\omega}$$

$$\begin{aligned} \epsilon^{ijk} \partial^j (\vec{u} \times \vec{\omega})^k &= \epsilon^{ijk} \partial^j \epsilon^{klm} u^l \omega^m = \\ &= (\delta^{il} \delta^{jm} - \delta^{im} \delta^{jl}) \partial^j (u^l \omega^m) = \partial^m (u^i \omega^m) - \partial^m (u^m \omega^i) \\ &= (\partial^m u^i) \omega^m + u^i \partial^m \omega^m - (\partial^m u^m) \omega^i - u^m \partial^m \omega^i \\ &\quad - u^m \partial^m \omega^i \end{aligned}$$

(  $\omega^m = \epsilon^{mpq} \partial p u^q$  )

or, in short  $\nabla \times (\bar{u} \times \bar{\omega}) = (\bar{\omega} \nabla) \bar{u} - (\bar{u} \nabla) \bar{\omega}$

$\frac{\partial \bar{\omega}}{\partial t} + (\bar{u} \nabla) \bar{\omega} = (\bar{\omega} \nabla) \bar{u} + \nu \Delta \bar{\omega}$

or  $\frac{D \vec{\omega}}{Dt} = \nu \Delta \vec{\omega} + (\vec{\omega} \nabla) \vec{u}$

- This is an interesting equ: -  
- for sphere's Stokes' flow

$\bar{\omega} = \omega_{\varphi} \bar{e}_{\varphi}$

$\neq \bar{u}$  is  $\varphi$ -independent

hence  $(\bar{\omega} \nabla) \bar{u} = 0$  } for 2d flows  
or } for unidirectional flows

$\frac{D \vec{\omega}}{Dt} = \nu \Delta \vec{\omega}$

this is really a "diffusion equ" for vorticity!!

$\left( \frac{\partial n}{\partial t} = D \Delta n \right)$   
↑  
diffusion coefft

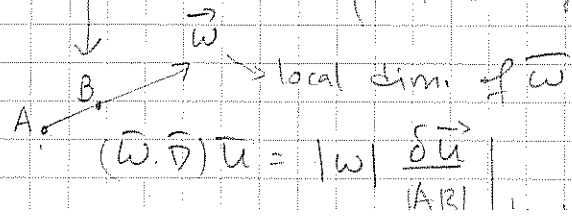
- written as

$\vec{\omega} = -(\bar{u} \nabla) \bar{\omega} + (\bar{\omega} \nabla) \bar{u} + \nu \Delta \bar{\omega}$

same as  $(\bar{u} \nabla) \bar{u}$

for velocity "convective" term  
→  $\bar{\omega} \neq 0$  cause of nonuniformity of  $\bar{u}$  along the flow

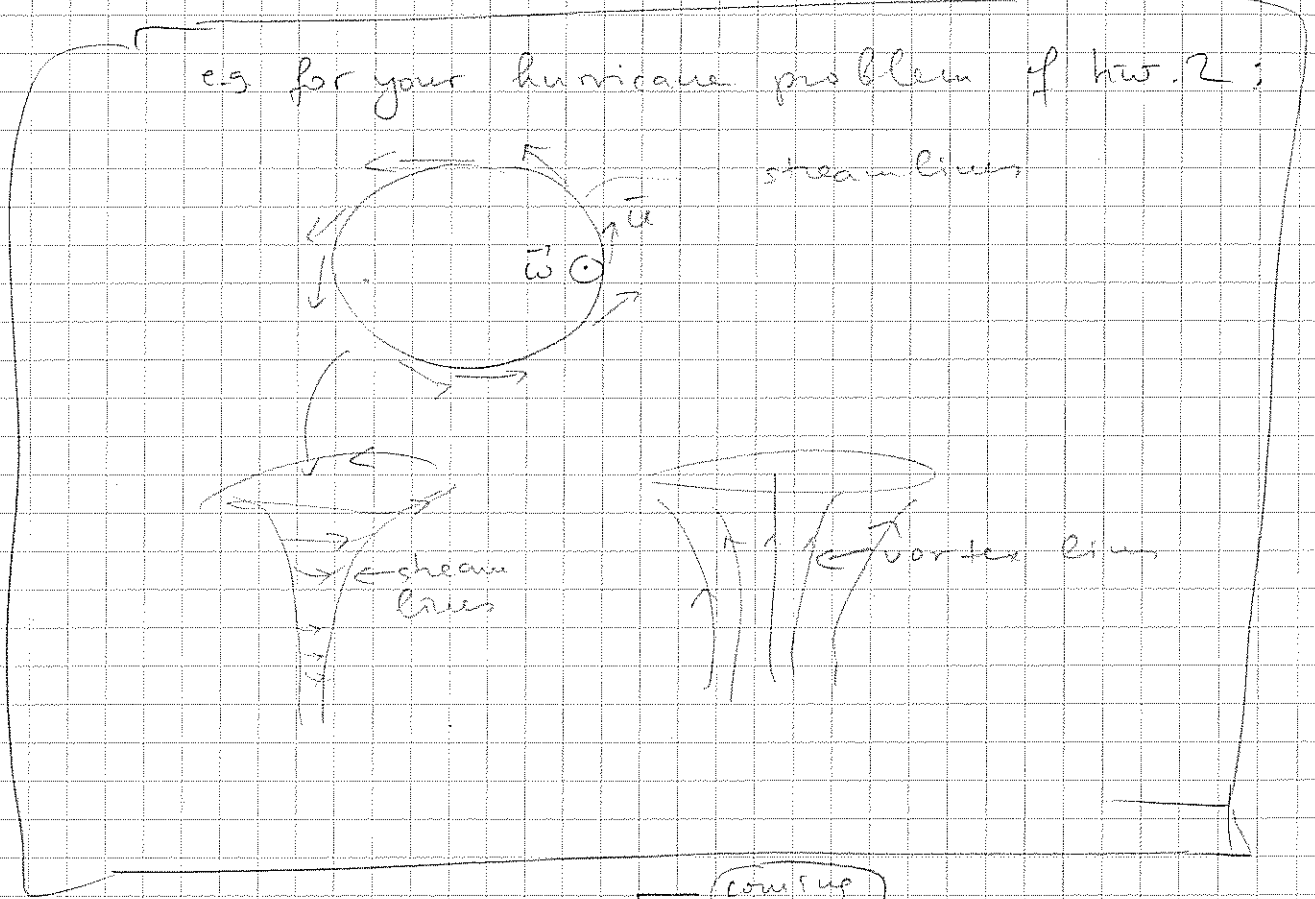
"diffusion" of  $\bar{\omega}$  (like "diffusion" of  $\vec{u}$ )  
(same coefft.  $\nu$ )



$\delta \bar{u} = \bar{u}_B - \bar{u}_A$

just like streamlines = lines s.t.  
tangent vectors are  $\vec{u}(\vec{x}, t)$   
at  $(\vec{x}, t)$

one can introduce vortex lines = lines s.t.  
tangent vector @  $\vec{x}, t = \vec{\omega}(\vec{x}, t)$

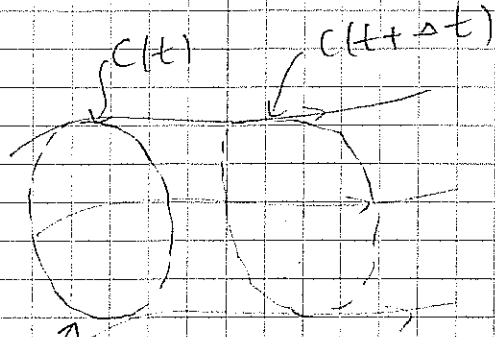


conclude

Concepts of vorticity & circulation play important role in inviscid fluid flows & air lift theory.

- Our plan:
- high-R  $\Rightarrow$  might as well take  $\nu = 0$
  - study simple 2d flow of Karman's lift theorem
  - implies paradoxes  $\Rightarrow$  boundary layers (irrelevant)
- ((that'll be all!))

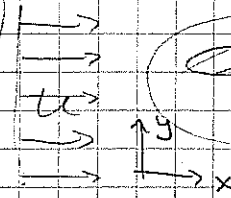
Circulation & vorticity:



material curve, closed

importance of  $\Gamma$ :

"Kutta-Joukowski lift theorem"



$$F_y = -\rho U \Gamma$$

$e \in C(t)$

every point move w/ fluid

according to:

$$\frac{d\vec{x}(t)}{dt} = \vec{u}(\vec{x}(t), t)$$

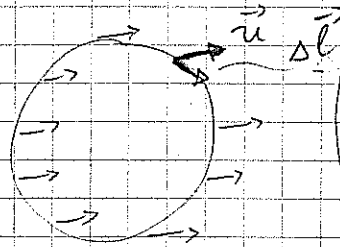
not necessarily stationary flow

"circulation"

$$\Gamma(t) = \oint_{C(t)} \vec{u} \cdot d\vec{\ell}$$

e.g.

$C(t)$



$$\Gamma = \sum_{C(t)} \vec{u} \cdot \Delta \vec{\ell}$$

$\Gamma$  depends on time because (a)  $\vec{u} = \vec{u}(\vec{x}, t)$

(b) points on contour move w/ flow

$$\frac{d\Gamma(t)}{dt} = \frac{d}{dt} \oint_{C(t)} \vec{u}(\vec{x}(t), t) \cdot d\vec{\ell}(t) =$$

$\vec{x} \in C(t)$

tangent vector to  $C(t)$  @  $\vec{x} \in C(t)$

$$= \oint_{C(t)} \frac{d}{dt} (\vec{u}(\vec{x}(t), t)) \cdot d\vec{\ell}(t) + \oint_{C(t)} \vec{u}(\vec{x}(t), t) \cdot \frac{d}{dt} (d\vec{\ell}(t))$$

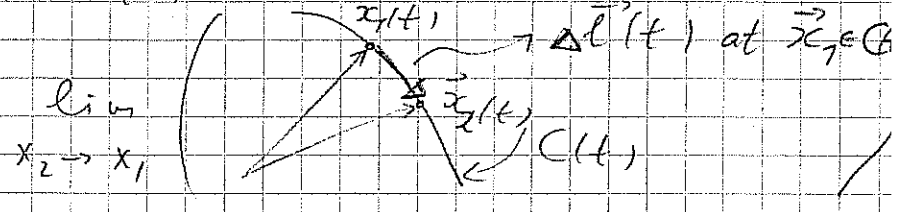
$$\frac{d}{dt} u^i(\vec{x}(t), t) = \frac{\partial u^i}{\partial x^j} \frac{\partial x^j}{\partial t} + \frac{\partial u^i}{\partial t}$$

$u^j$ , by e.o.u. of physical fluid element

$$= u^j \partial_j u^i + \dot{u}^i = \frac{D u^i}{D t}$$

?  $\frac{d}{dt} \vec{\ell}(t)$  ?

@ t:  $\Delta \vec{\ell}(t)$



$$\begin{aligned} \Delta \vec{\ell}(t + \Delta t) &= \vec{x}_2(t + \Delta t) - \vec{x}_1(t + \Delta t) \\ &= \vec{x}_2(t) + \Delta t \vec{u}(\vec{x}_2(t), t) \\ &\quad - \vec{x}_1(t) - \Delta t \vec{u}(\vec{x}_1(t), t) \end{aligned}$$

$$\Delta \vec{\ell}(t + \Delta t) = \Delta \vec{\ell}(t) + \Delta t (\vec{u}(\vec{x}_2(t), t) - \vec{u}(\vec{x}_1(t), t))$$

$$\Delta \ell^i(t + \Delta t) - \Delta \ell^i(t) = \Delta t (u^i(\vec{x}_2(t), t) - u^i(\vec{x}_1(t), t))$$

where  $x_2 \rightarrow x_1$

$$\begin{aligned} &= \Delta t (u^i(\vec{x}_1(t) + \Delta \vec{\ell}(t), t) - u^i(\vec{x}_1(t), t)) \\ &= \Delta t \frac{\partial u^i}{\partial x^j}(\vec{x}_1(t), t) \Delta \ell^j(t) \end{aligned}$$

so  $\frac{d \vec{\ell}}{dt} = (\Delta \vec{\ell} \cdot \vec{\nabla}) \vec{u}$



So --

$$\frac{1}{2} \partial_j (\vec{u}^2) dl^j = \frac{1}{2} d\vec{l} \cdot \vec{\nabla} \left( \frac{u^2}{2} \right) \quad (152)$$

$$\frac{d\Gamma}{dt} = \oint_{C(t)} \frac{D\vec{u}}{Dt} \cdot d\vec{l} + \oint_{C(t)} u^i \partial_j u^i dl^j$$

$$= \oint_{C(t)} \frac{\vec{F}}{\rho} \cdot d\vec{l} - \oint_{C(t)} \frac{1}{\rho} \vec{\nabla} p \cdot d\vec{l} + \oint_{C(t)} v \Delta \vec{u} \cdot d\vec{l}$$

let  $\vec{F} = -\vec{\nabla} \psi$   
 $+ p = \text{const}$

$$+ \oint_{C(t)} \vec{\nabla} \left( \frac{1}{2} \vec{u}^2 \right) \cdot d\vec{l}$$

$$\oint_{C(t)} \vec{\nabla} \psi \cdot d\vec{l} = 0$$

$\psi$  single valued

$$\Gamma = - \oint_{C(t)} \vec{\nabla} \left( \frac{p}{\rho} + \frac{1}{2} \vec{u}^2 \right) \cdot d\vec{l} + \int v \Delta \vec{u} \cdot d\vec{l}$$

if  $p$  &  $\vec{u}^2$  are single valued around  $C(t)$

$$\equiv 0.$$

$$\oint_C \vec{\nabla} f \cdot d\vec{l} = f(2) - f(1) = 0$$

since 1 = 2 closed contour

relation to  $\vec{\omega}$ :  $\vec{\nabla} \times \vec{\omega} = \vec{\nabla} \times (\vec{\nabla} \times \vec{u}) = -\Delta \vec{u}$

$$\Gamma = -v \oint_{C(t)} (\vec{\nabla} \times \vec{\omega}) \cdot d\vec{l}$$

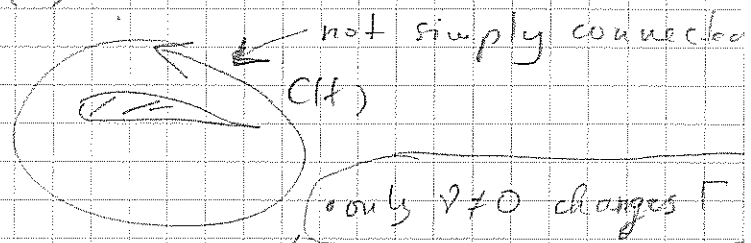
very general,  $\forall C(t)$  - closed s.t.  $\psi, p, \vec{u}^2$  are single valued

Moral  $\rightarrow$

$\dot{\Gamma} = 0$  for inviscid fluid

"Kelvin's circulation theorem"

- circulation around closed contours of material fluid elements is conserved (contour moves w/ fluid)
- again - single valuedness of  $\psi$  ( $\vec{F} = -\nabla\psi$ )  $\rho, \vec{u}^2$  used - but not simple connectedness of  $C(t)$ !



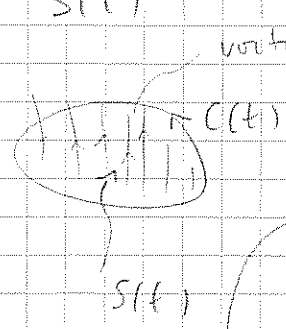
Once again:

$$\dot{\Gamma}(t) = \frac{d}{dt} \left( \int_{C(t)} \vec{u} \cdot d\vec{l} \right) = -\nu \int_{C(t)} (\nabla \times \vec{\omega}) \cdot d\vec{l}$$

$$\Gamma = \int_{C(t)} \vec{u} \cdot d\vec{l} = \int_{S(t)} \nabla \times \vec{u} \cdot d\vec{S} = \int_{S(t)} \vec{\omega} \cdot d\vec{S}$$

- $\dot{\Gamma}$  only depends on  $\nabla \times \vec{\omega}$  near  $C(t)$  (i.e. locally)
- even for viscous fluid, if  $\nu$  is small (high R)  $\nabla \times \vec{\omega}$  is small:  $\dot{\Gamma} \approx 0$
- generally  $\dot{\Gamma}$  will be appreciable only where  $\nabla \times \vec{\omega}$  is substantial (to overcome  $\nu \rightarrow 0$ )

$\Rightarrow$  near boundaries  $\Leftrightarrow$  where  $\vec{\omega}$  is created



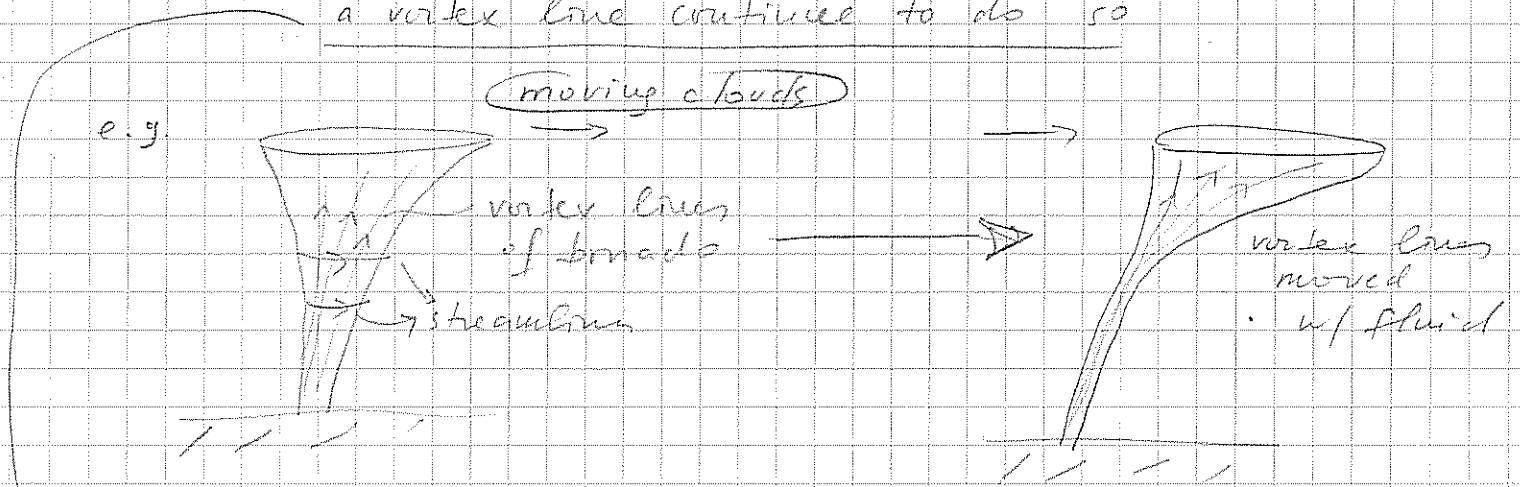
$\Gamma =$  total vorticity inside any fluid surface w/ boundary  $C(t)$

Ampere's law  $\oint_C \vec{A} \cdot d\vec{l} = \int_S \vec{B} \cdot d\vec{S}$

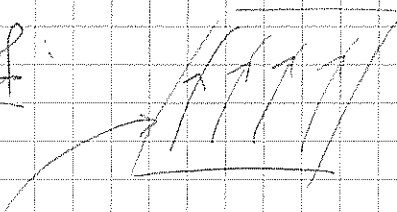
the conservation of circulation of an inviscid incompressible fluid combined w/ the fact that "vortex lines move w/ the fluid" has some powerful consequences

↳ aka Helmholtz vortex theorem

what it says is that fluid elements that lie on a vortex line continue to do so



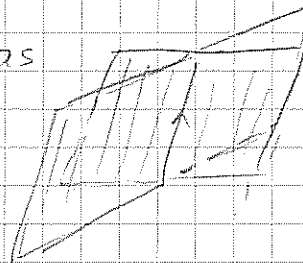
to prove:



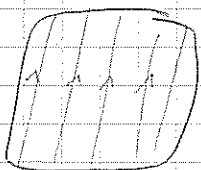
vortex surface: every element is a vortex line

always can view vortex line as

let  $C(t)$  - a contour lying on a vortex surface



intersection of two vortex surfaces



$$\Gamma(t) = 0 \text{ since } \Gamma = \int \vec{\omega} \cdot d\vec{S} = 0 \quad (\vec{\omega} \perp d\vec{S})$$

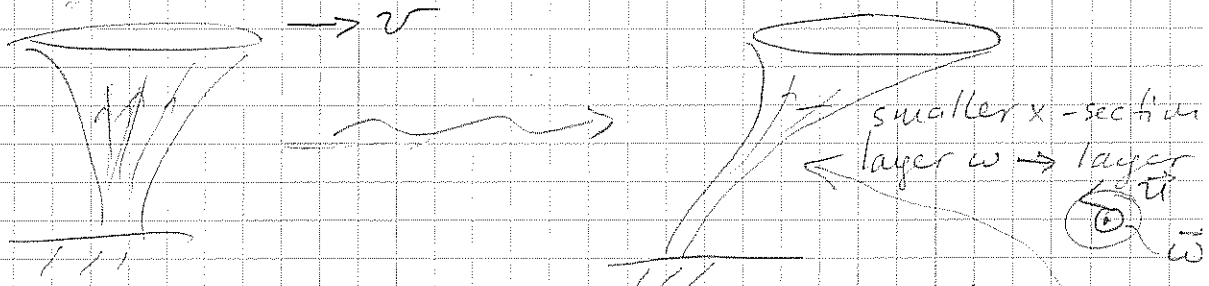
now since  $\dot{\Gamma} = 0$ ,  $\forall \Gamma = 0 \quad \forall C(t) \in (\text{vortex surface})$

$\Rightarrow \vec{\omega} \perp d\vec{S} \quad \forall t \Rightarrow$  a vortex surface remains a vortex

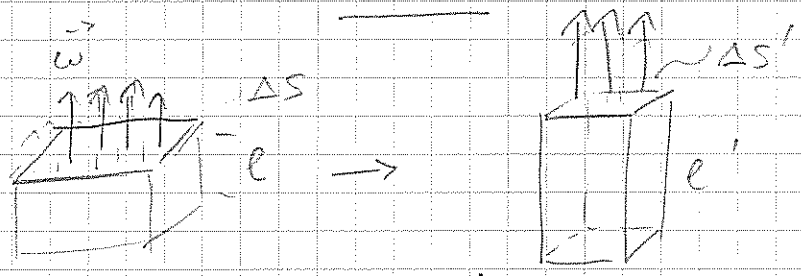
surface as time goes on  $\rightarrow$  & this holds for any vortex surface

Hence, the intersection of two vortex surfaces (i.e. our vortex line) will remain the intersection of two vortex surfaces  $\Rightarrow$  "vortex line remains a vortex line" or "physical fluid element that lie on a vortex line at some  $t$  remain on the vortex line at later  $t$ 's" — so  
"vortex lines move w/ flow of fluid"  
 (incompressible, inviscid)

Now back to our tornado — since v-x lines move w/ fluid



motion of clouds stretches the vortex



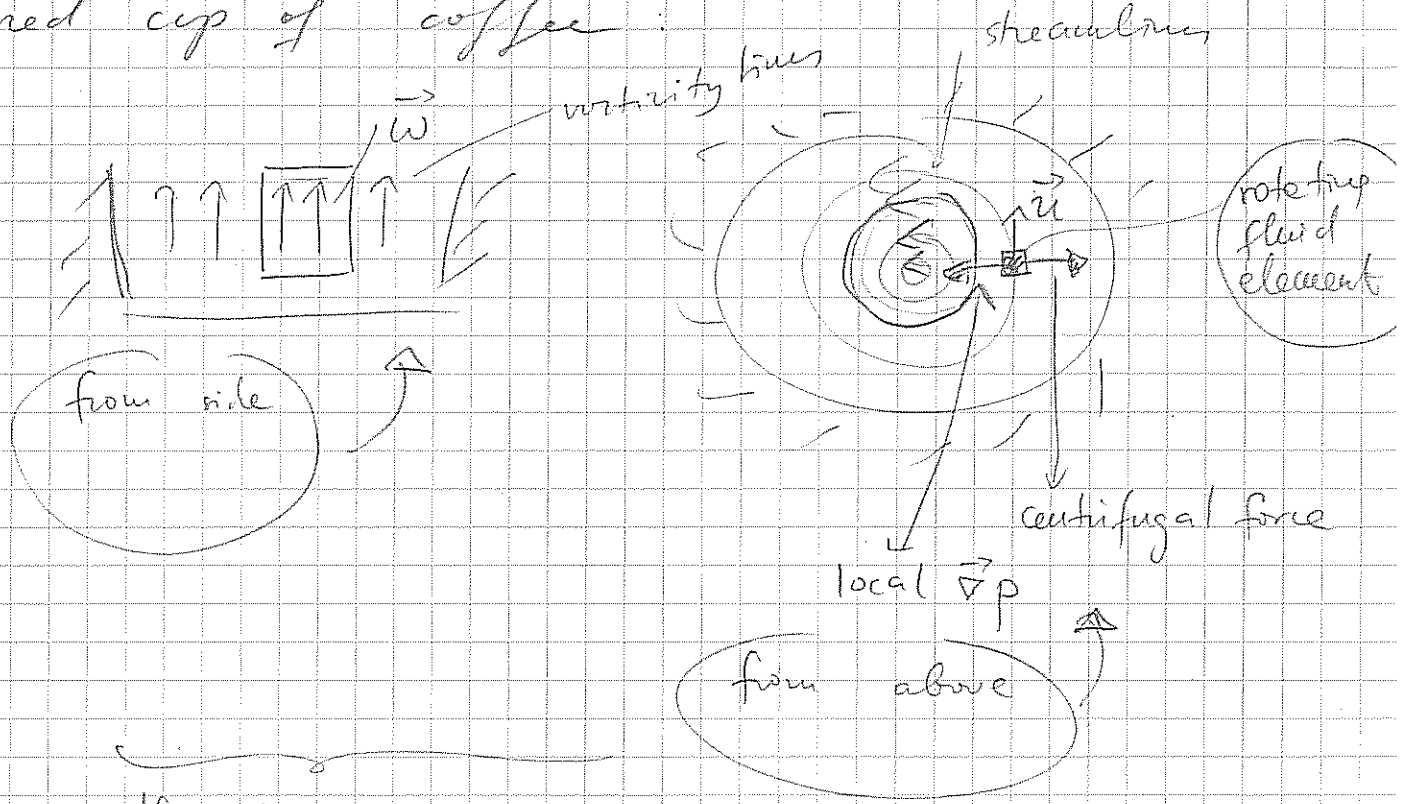
$$\Delta s' \cdot e' = \Delta s \cdot e \Rightarrow e \uparrow \rightarrow \Delta s \downarrow$$

$$\text{but } \Gamma \sim \omega \Delta s \Rightarrow \Delta s \downarrow \rightarrow \omega \uparrow$$

$\Rightarrow$  stretching a vortex  $\Rightarrow$  increased  $\vec{\omega}$

or v.v. compressing a vortex  $\Rightarrow$  decreased  $\vec{\omega}$

the latter case ("compressing" or "shortening" of vortex) is responsible for spin-down in a stirred cup of coffee:



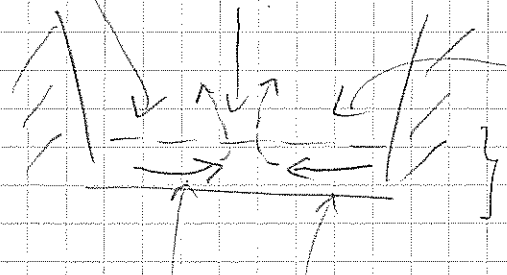
this is OK

far enough from boundaries, where  $\nabla$  is important

pressure higher

pressure lower

pressure higher



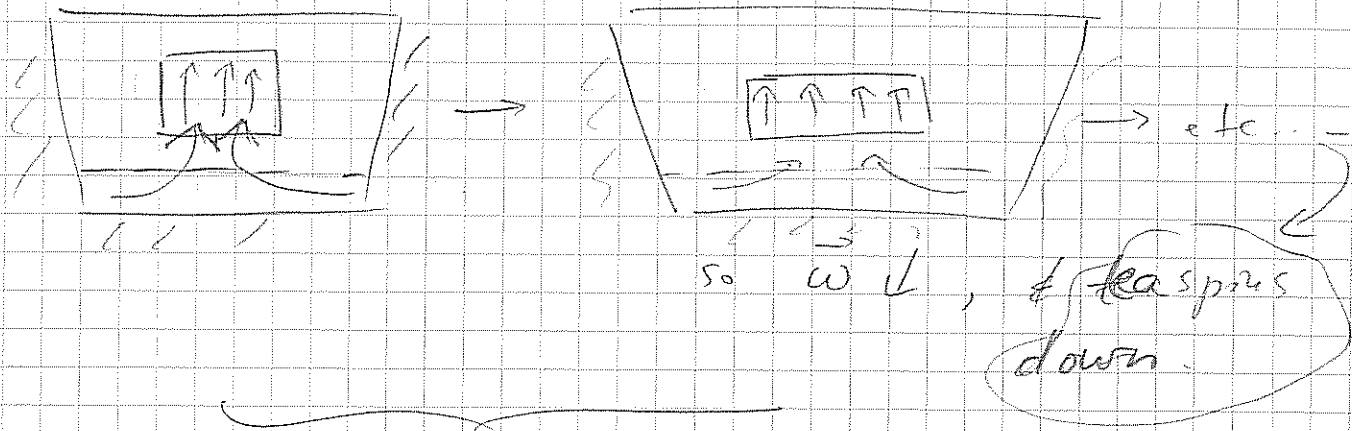
balance between  $\nabla p$  & centrifugal force near bottom:  $\nabla p$  pushes.

flow of bottom layer due to  $\nabla p$

bottom layer inwards

is inward & upwards @ center bottom - then carry much less vorticity (as bottom viscous layer rotates <sup>more</sup> slowly) so vorticity near bottom is decreased  $\rightarrow$

In effect, water lines become shorter



This story can be made more precise by the study of boundary layers (we'll do a bit of qualitative analysis later).

Before that, let's do some classic FM "stuff"

2D inviscid, incompressible & irrotational flow & the Zhukovskii lift theorem.

- we've almost done all preparatory work, since we already introduced the stream function ---